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# Use of Ammonia and Nitrate Sensors for Activated Sludge Aeration Control

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# Overview

## Sensors Available

- Optical
  - Nitrate / Nitrite
- Ion Selective Electrodes (ISE)
  - Ammonium / Nitrate

## ISE Theory of Operation

- Relationship of Ammonia & Ammonium
- Potassium & Chloride Compensation electrodes

## Biological Nitrogen Removal basics

## Control Strategy

- Ammonium to control aeration rates
- Nitrate to control recycle rates

## Case Studies using Ammonia to control aeration rates

The background features a blue gradient that transitions from a lighter shade at the top to a darker shade at the bottom. A white line starts at the top left, curves upwards to the right, then levels off horizontally, and finally curves downwards to the right, creating a shape that resembles a stylized 'S' or a path. The text 'Sensors Available' is centered in the upper half of the image in a white, sans-serif font.

# Sensors Available

# Optical

Based upon principle that nitrates and nitrites absorb certain wavelengths of light – a miniature spectrophotometer

- **Advantages:**

- No electrodes to replace
- Continuous ultrasonic self cleaning

- **Disadvantages**

- Cost 3x of ISE
- No ammonia measurement



# Ion Selective Electrode (ISE)

Based upon principle that electrodes generate a mV output proportional to compound of interest

- **Advantages:**

- Low cost
- Measure ammonium and nitrate in one package

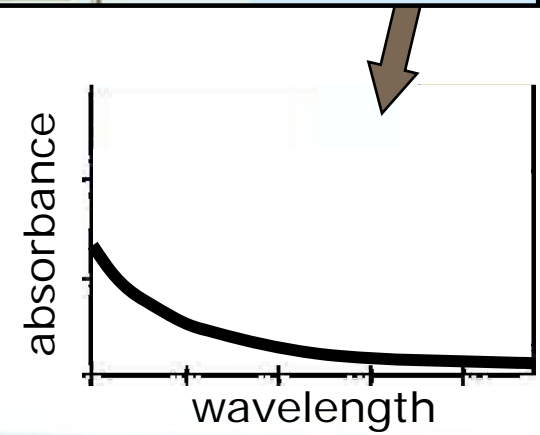
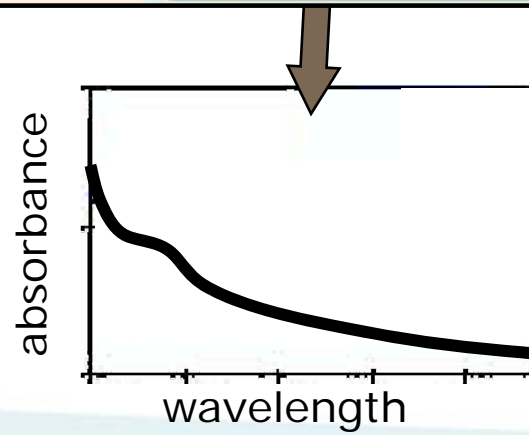
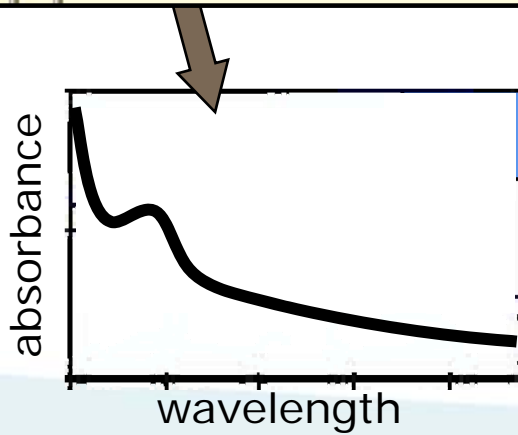
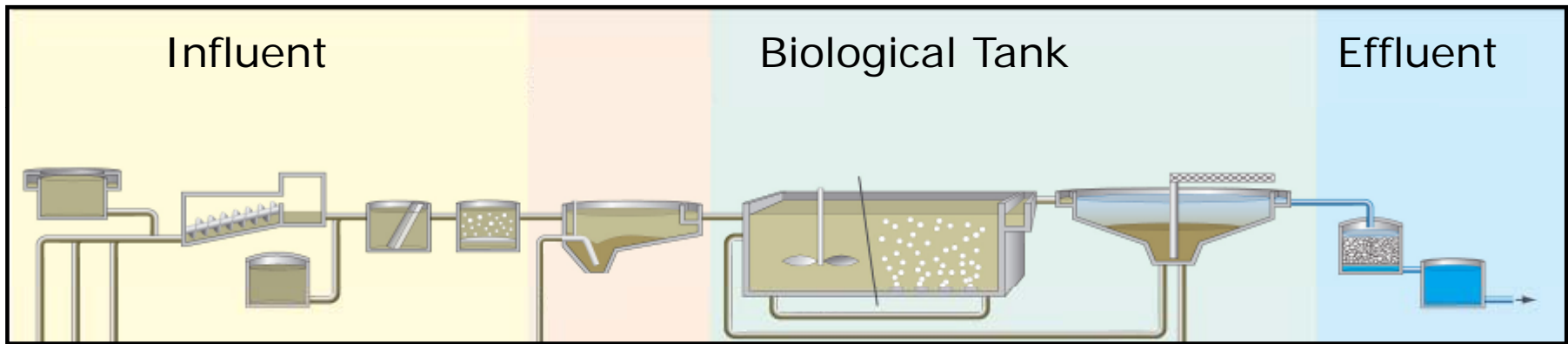
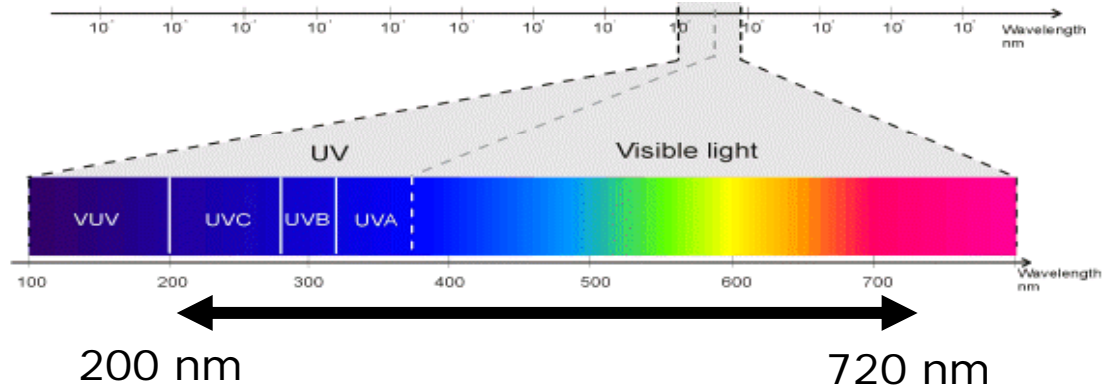
- **Disadvantages**

- Requires manual or air cleaning
- Requires replacement electrodes every other year



# Theory of Operation

# Optical



# Continuous Ultrasonic Self Cleaning

No maintenance  
Continuous cleaning  
No compressed air requirement



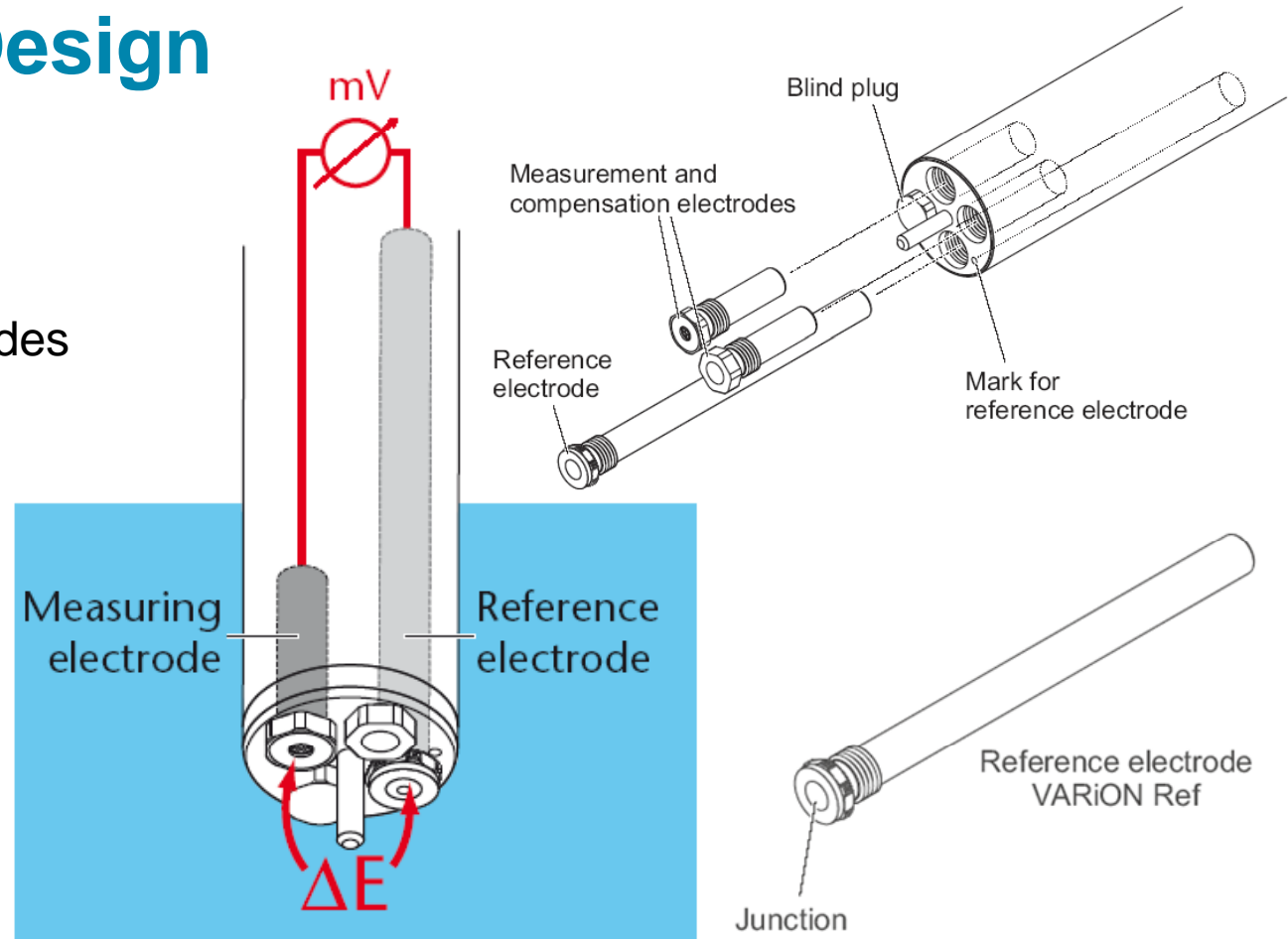
After 1 week of installation,  
post trickling filter,  
pre aeration contact chamber



# ISE Sensor Design

## Four Measuring Electrodes

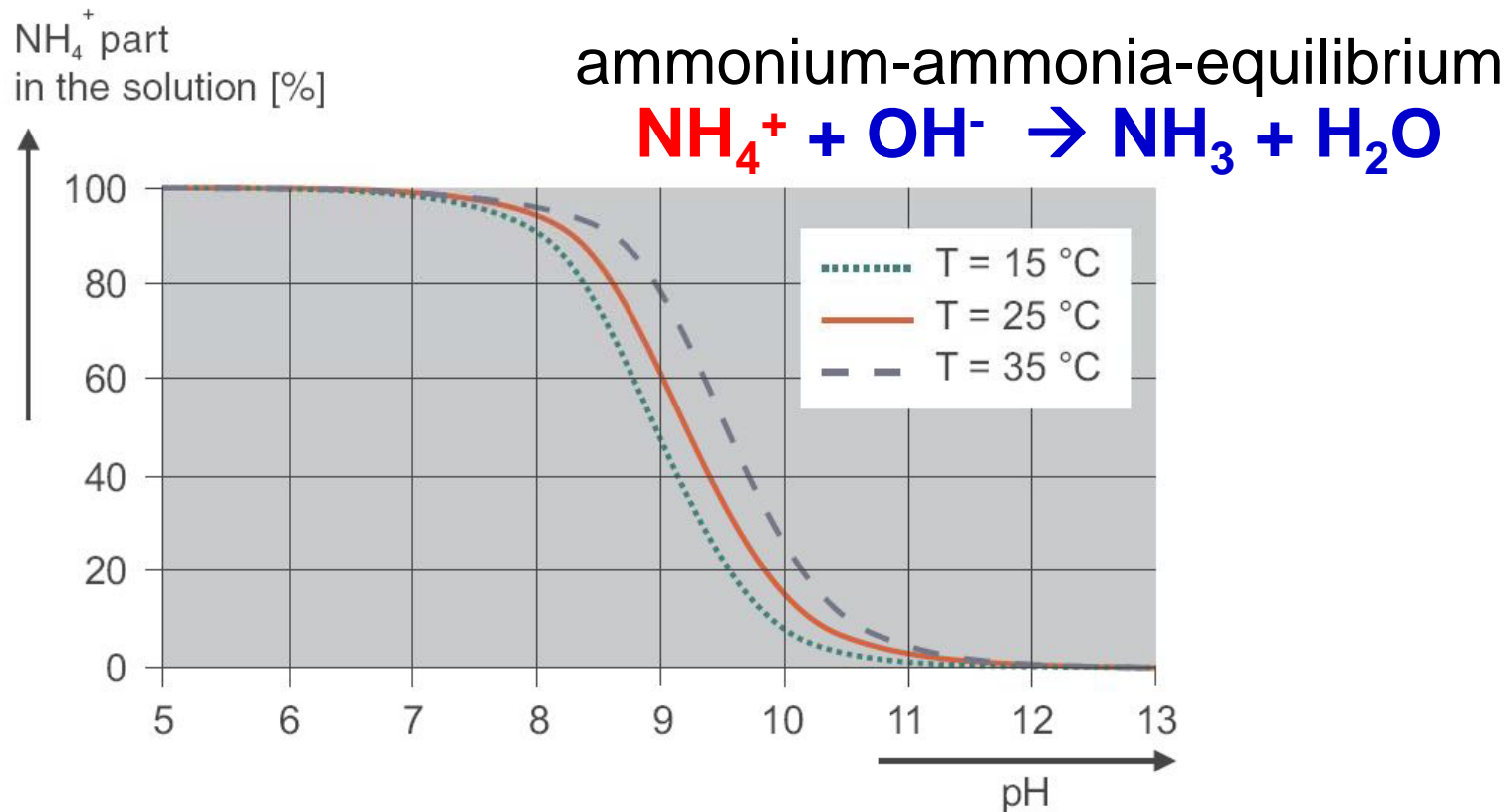
- NH<sub>4</sub>-N
- NO<sub>3</sub>
- K
- Cl



All electrodes can be exchanged individually

New electrodes are automatically recognized

# Relationship of Ammonia & Ammonium



- Uncompensated  $\text{NH}_4^+$  detection good up to approx. pH 8.5
- pH values > 8.5  $\text{NH}_4^+$ : detection requires pH compensation

# The need for Compensation Electrodes

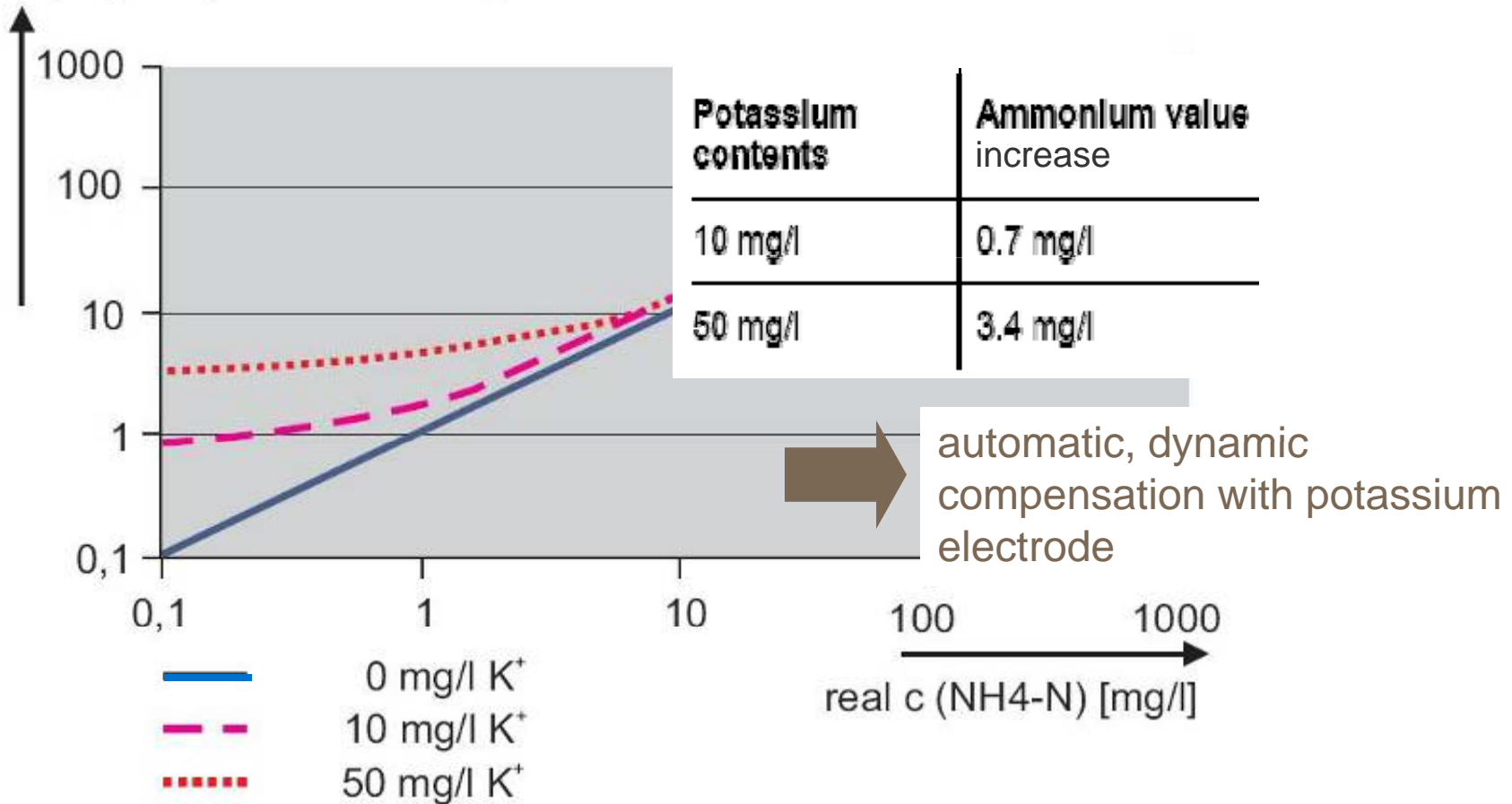
ISE's have known and predictable interferences:

- Ammonium's primary interference is Potassium
- Nitrate's primary interference is Chloride



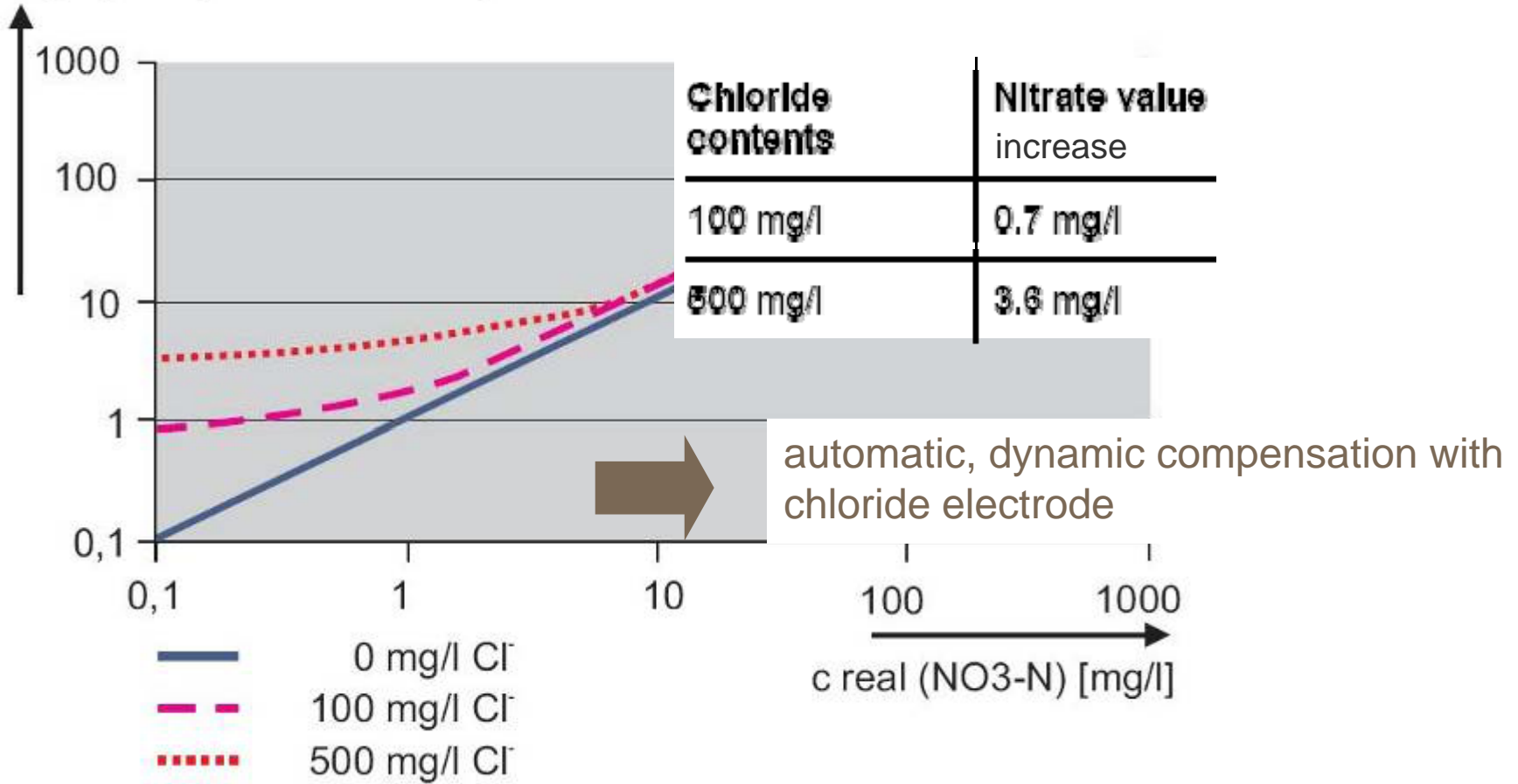
# NH<sub>4</sub>: Interference mainly by Potassium ions

c (NH<sub>4</sub>-N) [mg/l]  
displayed by the VARiON system



# NO<sub>3</sub>: Interference mainly by Chloride ions

c (NO<sub>3</sub>-N) [mg/l]  
displayed by the VARiON System



# Robust electrodes

Metal grid effectively protects the sensitive ISE membranes from damage due to physical cleaning

Easily clean electrodes, even with plastic brushes

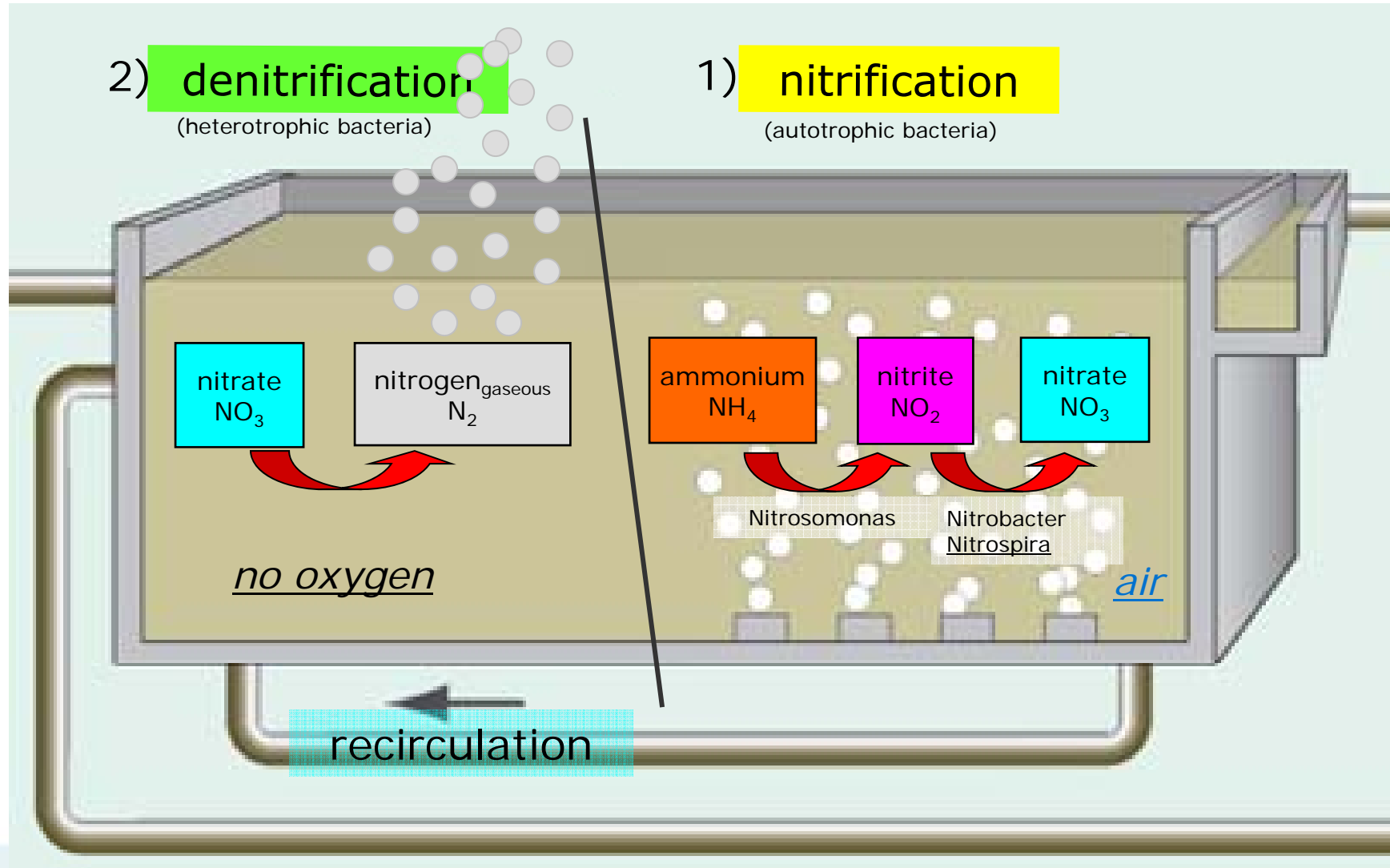


Important:  
do not use detergents/soaps for cleaning, as they destroy  
membranes

use only warm water and, e.g., a toothbrush

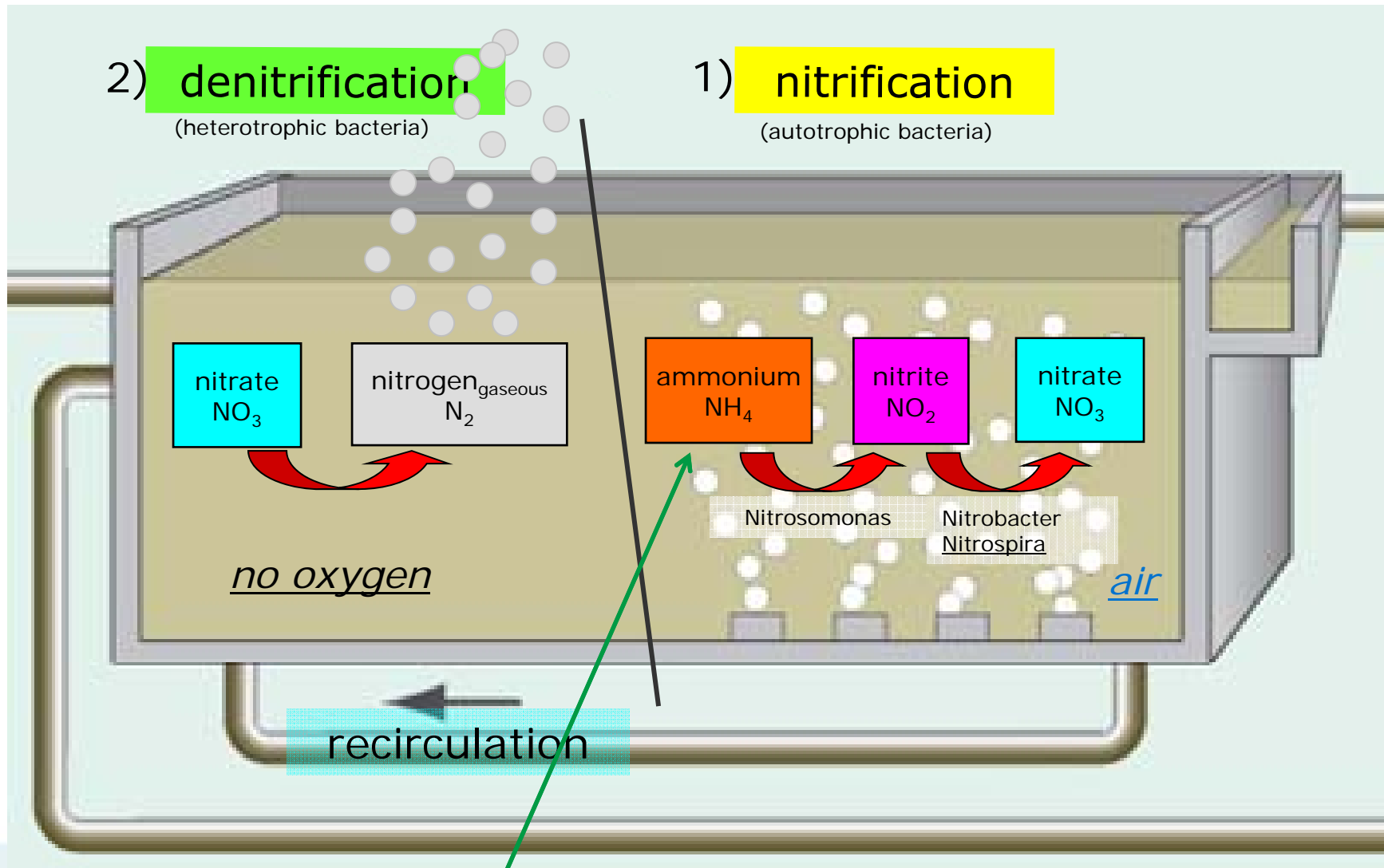
# Biological Nitrogen Removal basics

# Biological Nitrogen Removal



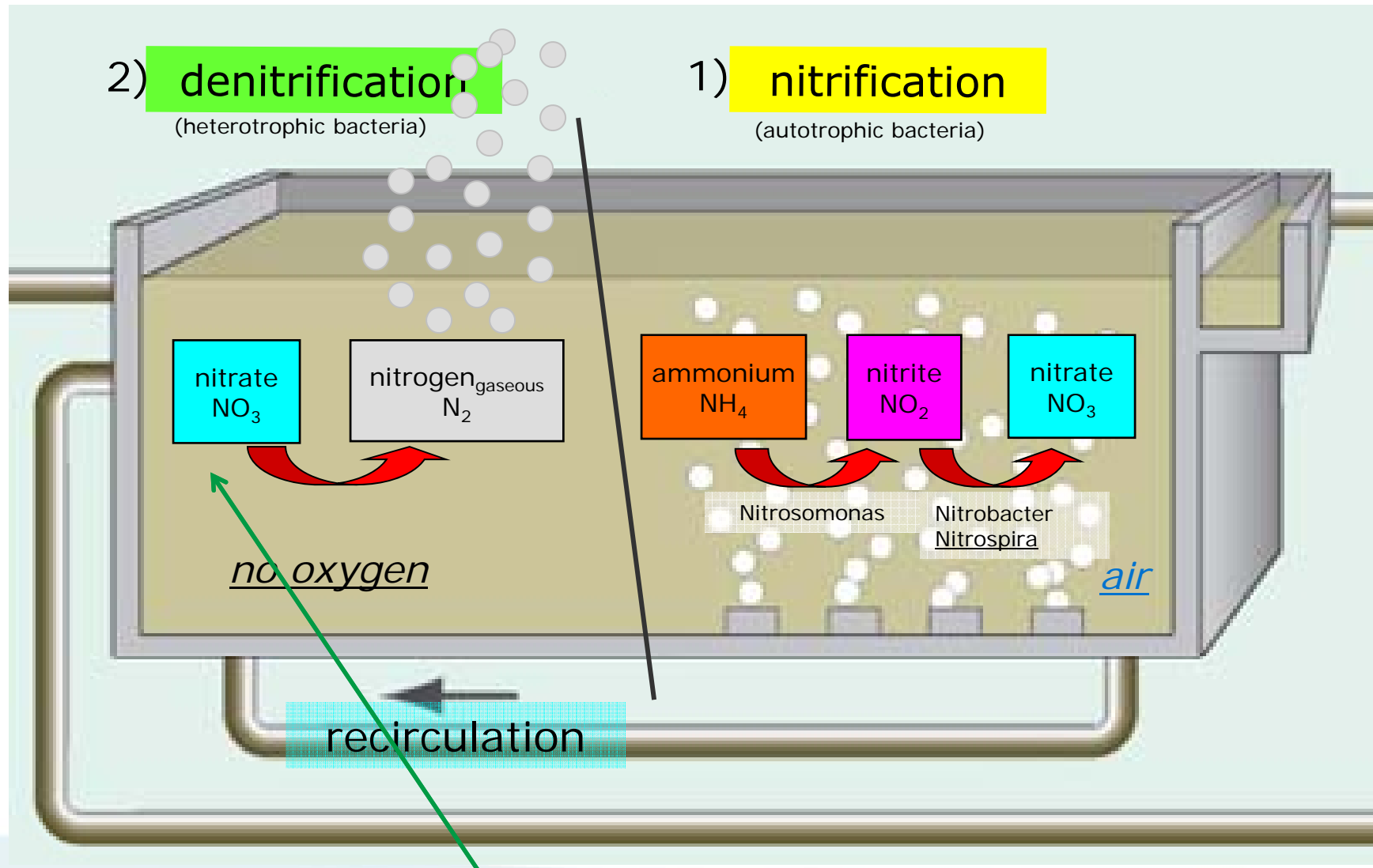


# Ammonia control objective



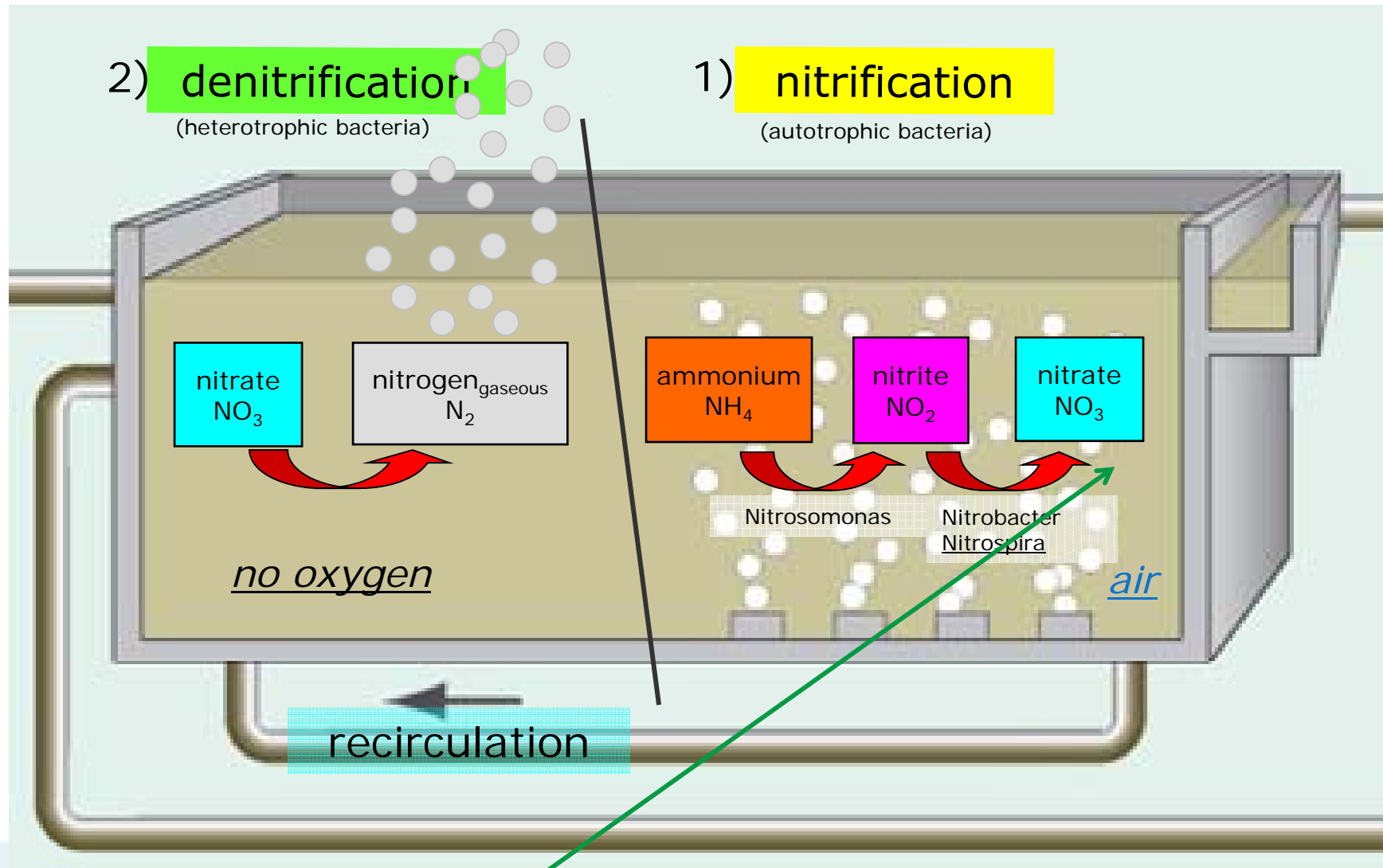
As Ammonia level rises above setpoint, increase air supply rate to further nitrification

# Nitrate control objective via aeration



As nitrate level rises above setpoint, decrease air supply rate to further denitrification

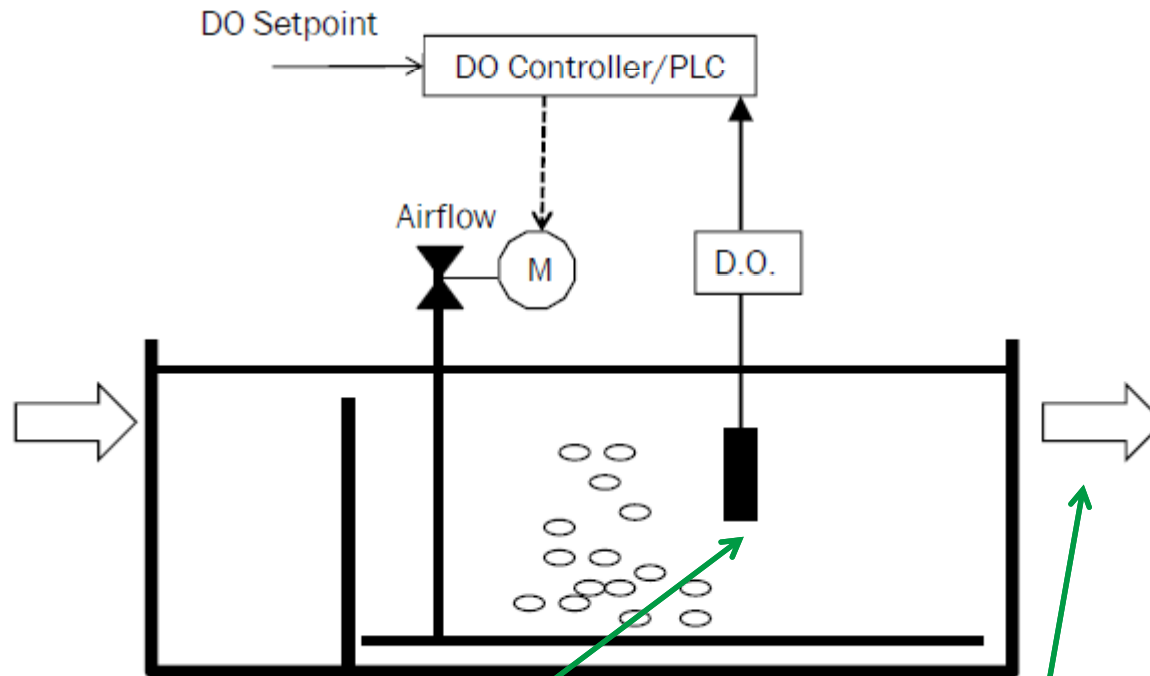
# Nitrate control objective via recirculation



Use of Nitrate to control Internal Mixed Liquor flow rate

# Ammonia based Control Strategy

# Typical Aeration Basin Control Strategy - DO



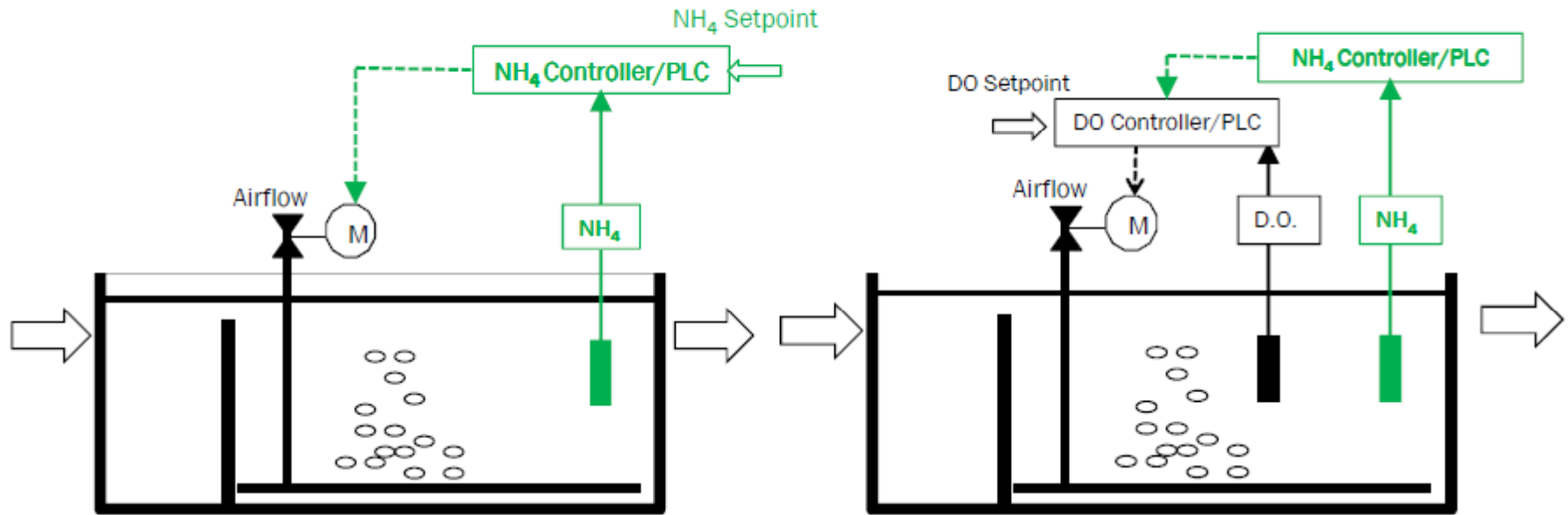
DO setpoint chosen to minimize historical  $\text{NH}_4$  breakthrough.

# Objective of Ammonia based Aeration control

Aeration control based on ammonia measurement essentially is applied for one of two reasons:

- Limiting aeration: Aeration is limited to prevent complete nitrification. The potential benefits include energy savings, increased denitrification, and in some cases improved bio-P performance.
- Reducing effluent ammonia peaks: Aeration is manipulated to reduce the extent of effluent ammonia peaks.

# Ammonia/Aeration Basin Control Strategies



Ammonia Feedback Control

Cascade to DO set point (or visa versa)

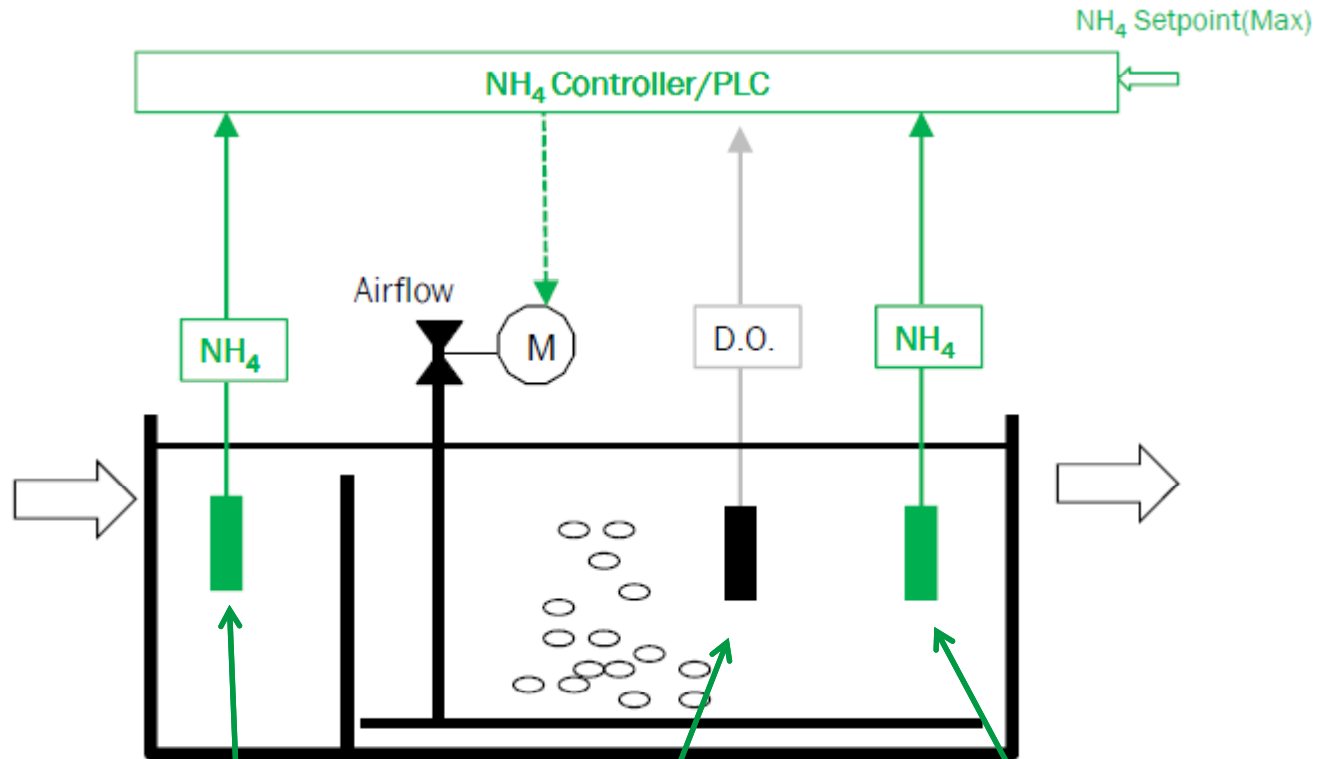
## Example

$\text{NH}_4 < 1.5$  mg/L then DO setpoint = 0.5 mg/L

$\text{NH}_4 > 1.6$  mg/L then DO setpoint = 2.0 mg/L

Cascade setpoint control slow to adjust DO

# Ammonia Feed Forward – Feedback Control

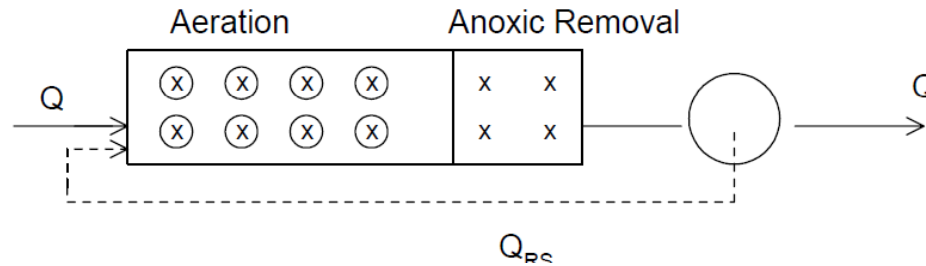


Upstream NH<sub>3</sub>. Min & Max limiting DO. Downstream NH<sub>4</sub>.

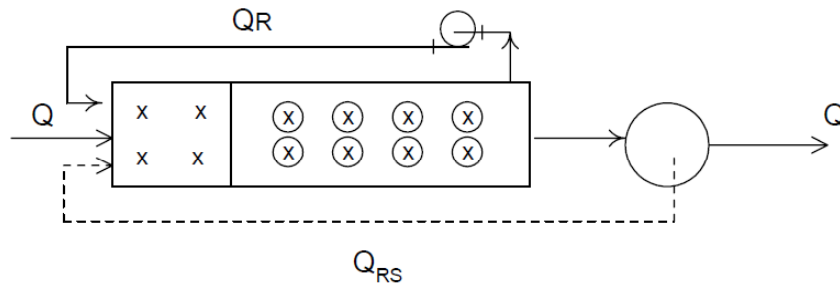


# Types of Single Sludge Nitrogen Removal

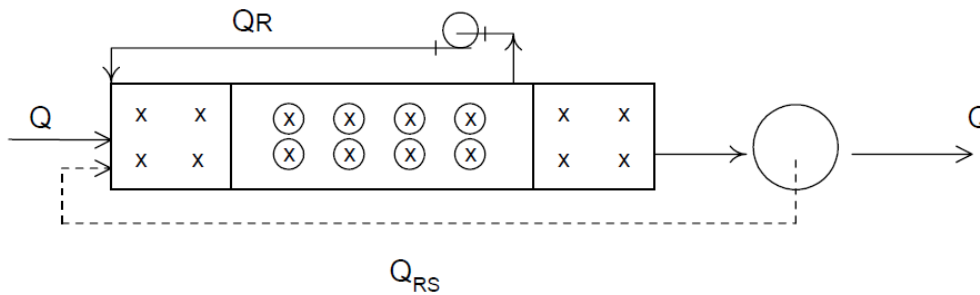
Post-denitrification



Pre-denitrification



Pre and Post-denitrification

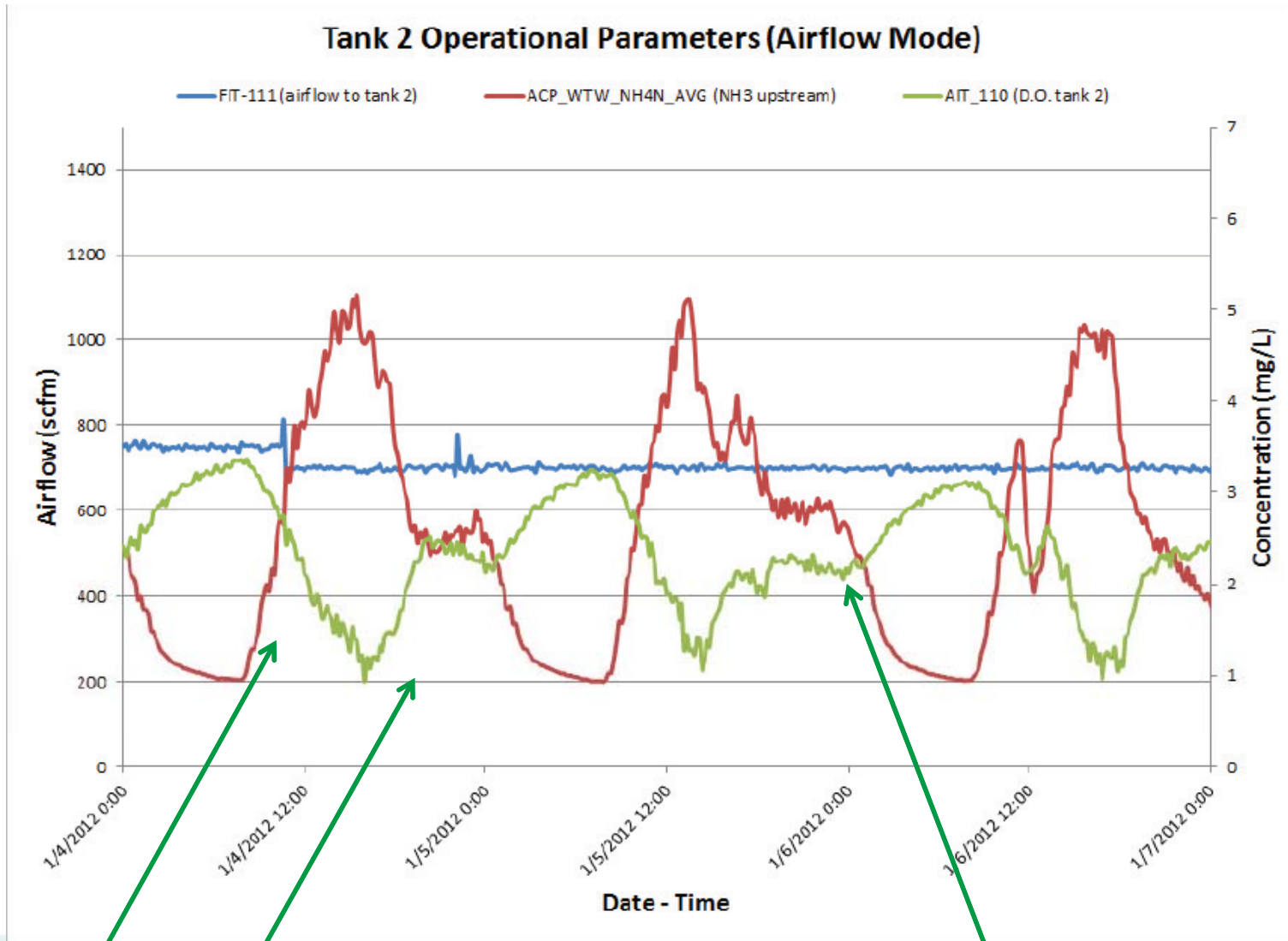


# Case Study: Wheaton Sanitary District

# Aeration Basin Instrumentation

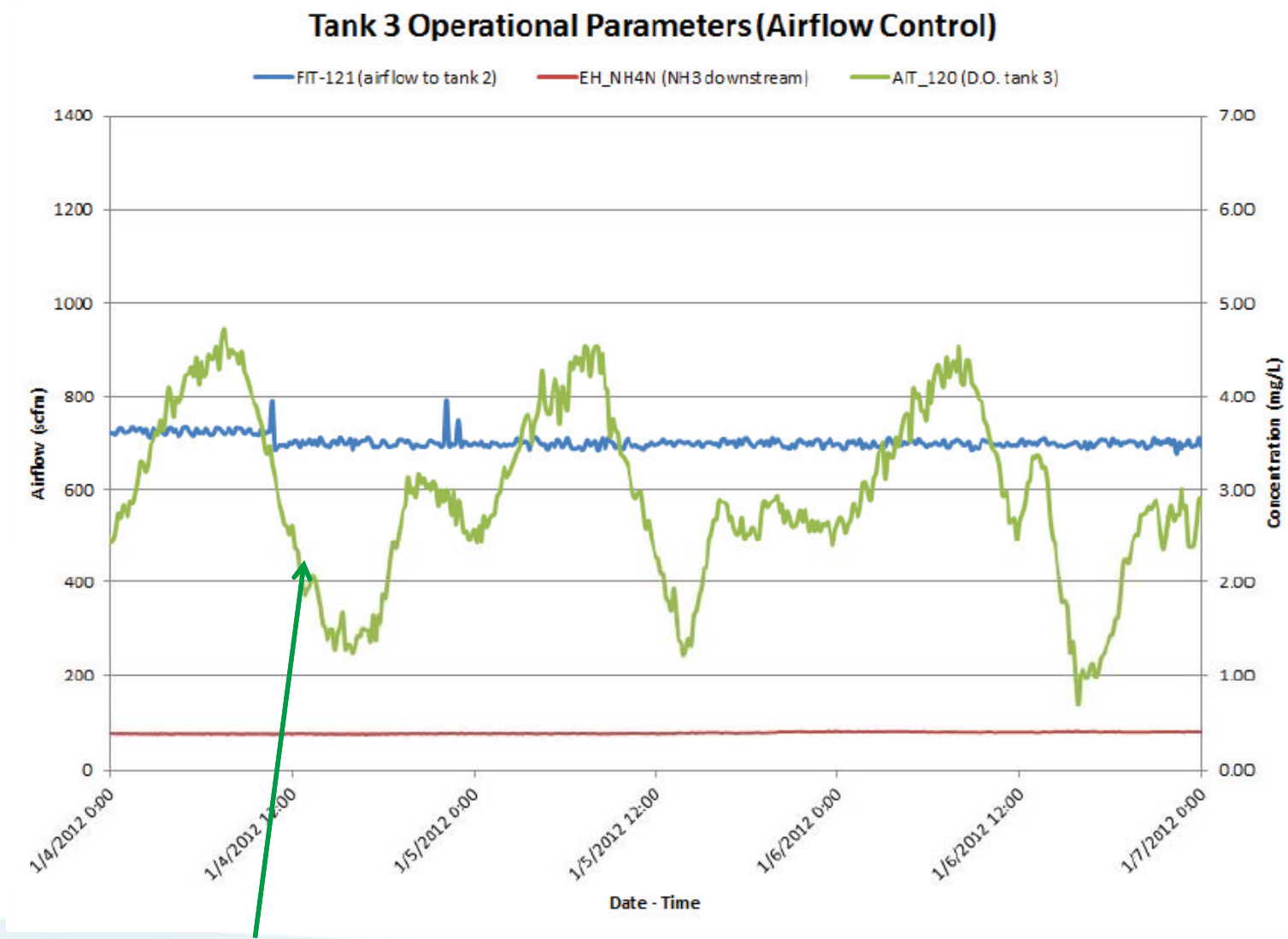


# Constant Airflow Mode - upstream



NH<sub>3</sub> and DO are inversely proportional. DO response to NH<sub>3</sub> is fast.

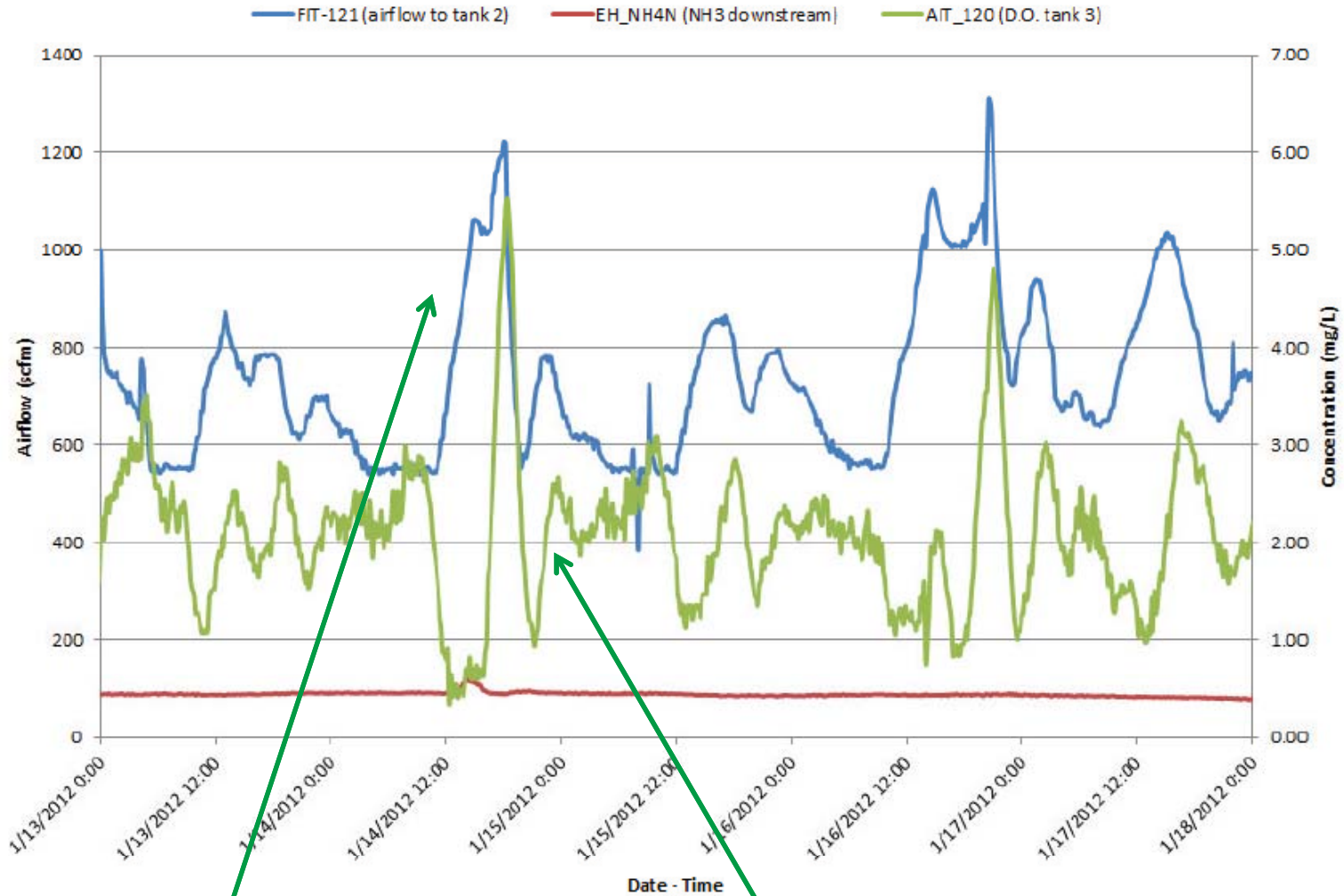
# Constant Airflow Mode – downstream



DO swings based upon NH<sub>3</sub> loading at influent

# DO control mode – 2ppm setpoint

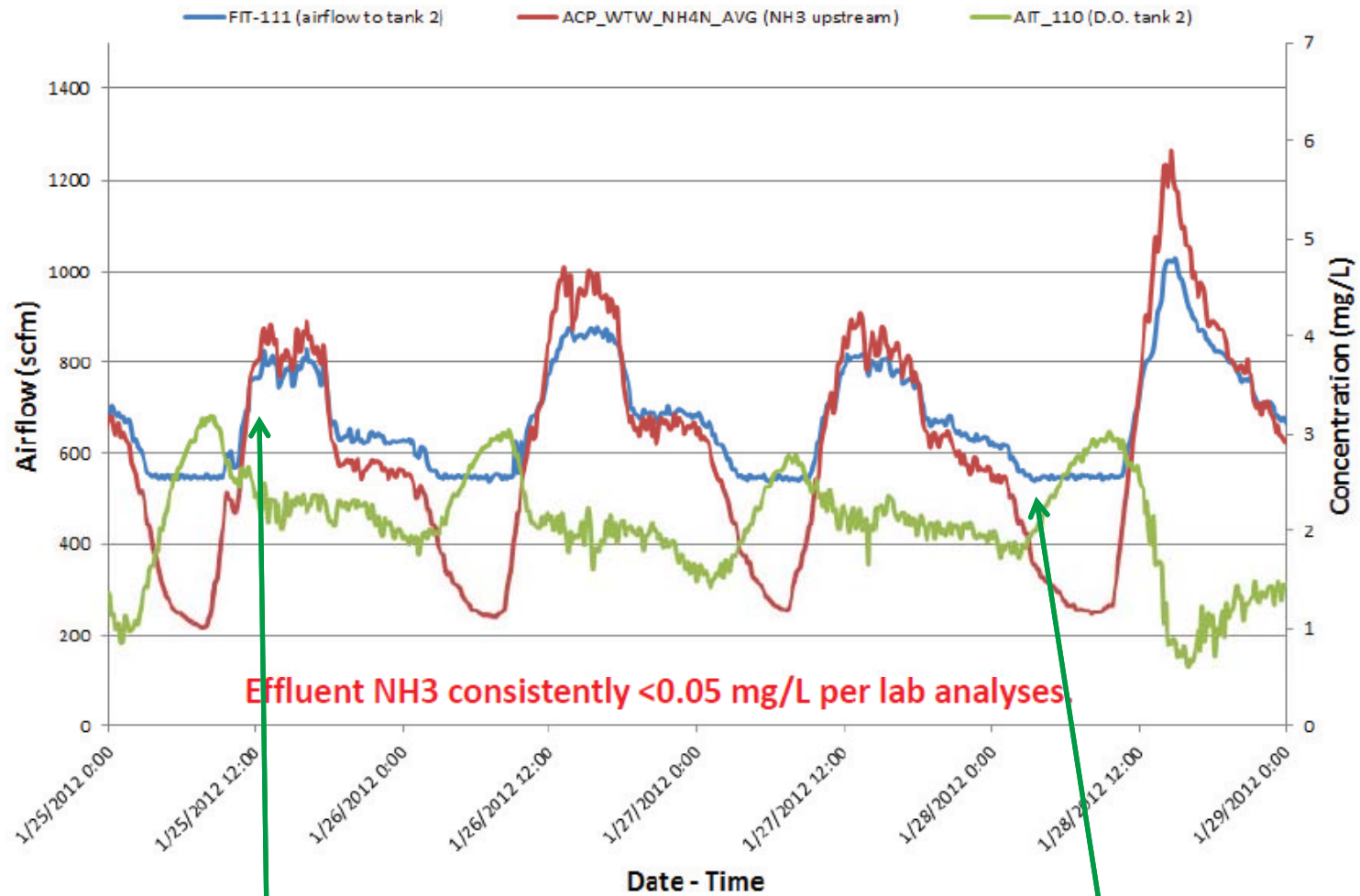
## Tank 3 Operational Parameters (D.O. Control)



Airflow inversely proportional to DO. Note NH<sub>3</sub> breakthrough.

# NH<sub>3</sub> Predictive Control

## Tank 2 Operational Parameters (Predictive NH<sub>3</sub> Control)

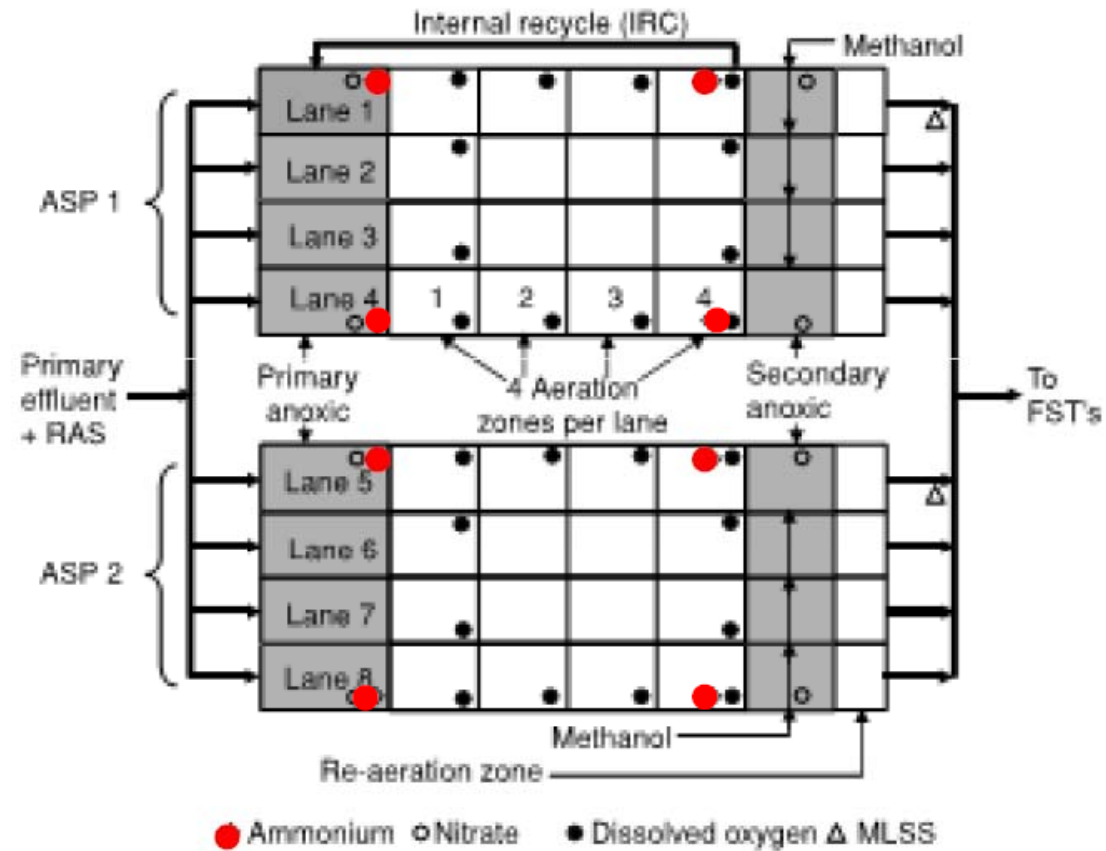


Airflow proportional to NH<sub>3</sub> concentration. Note lower limit on airflow for mixing.

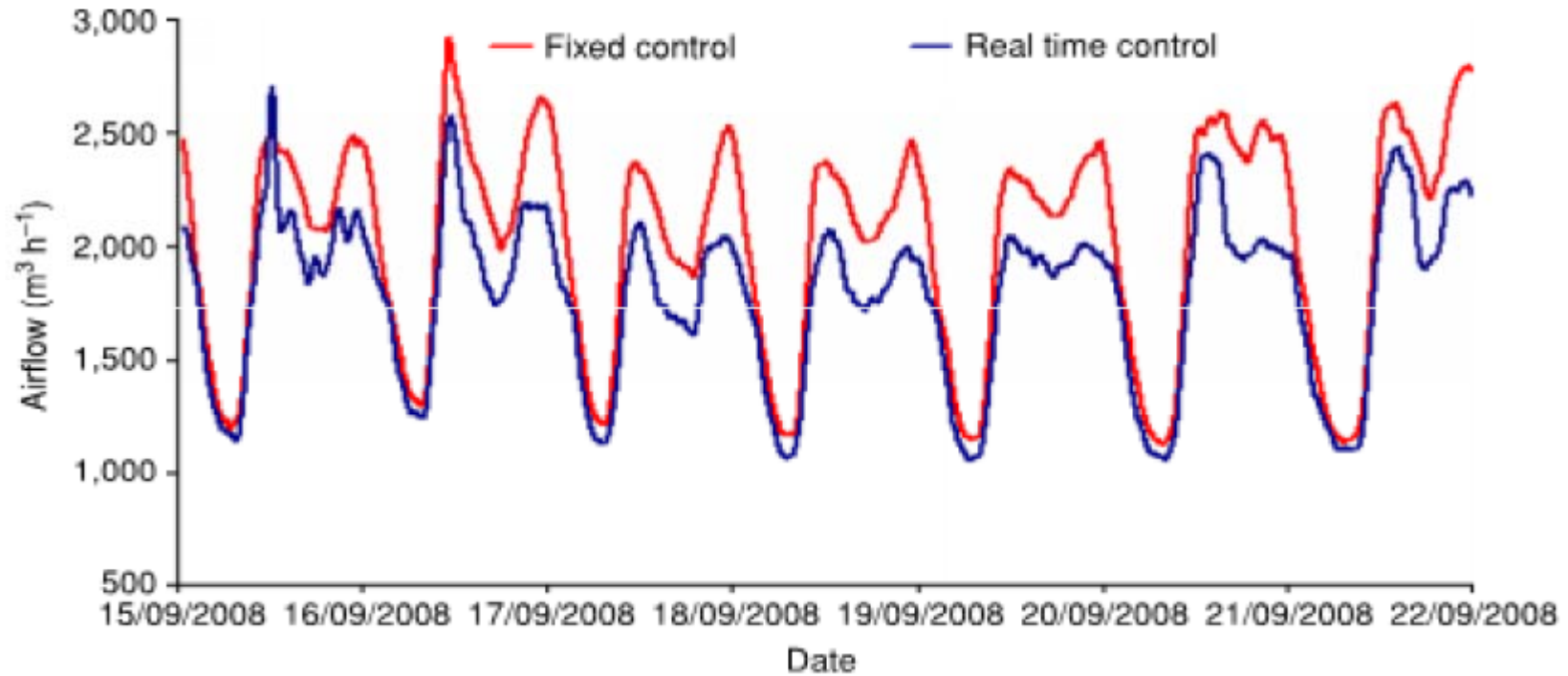
# Case Study: U.K. 4 Stage Bardenpho



# Plant Layout and Sensor Location

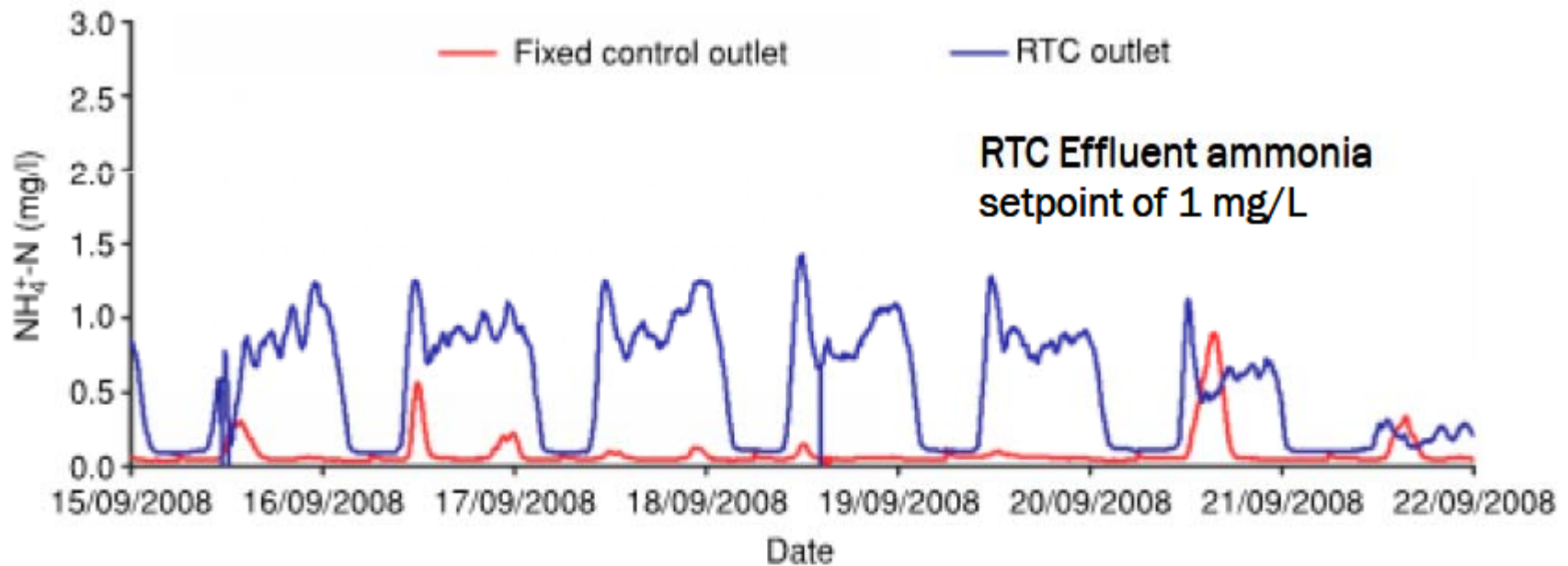


# DO setpoint vs Predictive NH4 Control



20% airflow savings overall

# Effect of Limiting Aeration preventing Complete Nitrification



# Case Study Summaries - Cons

- Need reliable and accurate sensors – test sensors for requirements
- Control can be more complex
  - Sensor outlay and maintenance
  - More monitoring
  - More maintenance (0.5 to 3 hours/week/device)
  - Cascade loops – lag times/fine tuning
  - Historical treatment or process model algorithms
- Blower turndown critical but must maintain minimum airflow for mixing
- Low D.O. bulking a concern—especially if D.O. <2.0 mg/L

# Case Study Summaries - Pros

- Switching to  $\text{NH}_3$  control can decrease airflow by 20%
- More stable effluent D.O. concentrations
- Allows for Limiting Aeration preventing complete nitrification to further increase savings
- Feed-forward provides greater safety w.r.t. peak loadings
- More stable effluent ammonia in high flows
- Depending on the starting conditions, even the simplest control (e.g. 1-point D.O. control) can provide significant energy savings
  - Take advantage of the low end of the blower curve
  - Minimal cost of implementation (VFD, in-tank instrumentation, programming)

# QUESTIONS



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